

# Validation of Models Simulating **Capillary and Dissolution Trapping** During Injection and Post-Injection of CO<sub>2</sub> in Heterogeneous Geological Formations Using Data from **Intermediate Scale Test Systems**

(DE-FE0004630)

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National Energy Technology Laboratory  
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Developing the Technologies and  
Infrastructure for CCS  
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# Presentation Outline

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- ❑ **Project Overview** - Goals & Objectives
  - Benefits of technology
  - Project status
- ❑ **Key questions and knowledge gaps**
  - Successful storage
  - Role of models in design
  - Conceptualization and key questions
- ❑ **Objectives and tasks**
- ❑ **Multi-scale physical and numerical modeling approach**
  - Experimental methods
- ❑ **Technical progress and results**
  - Experimental results
  - Modeling results
- ❑ **Findings**
- ❑ **Future Plans**
- ❑ **Appendix**

# Benefits of Technology to the Program

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- ❑ **Improve/develop and validate models** by using the data generated in intermediate-scale laboratory test systems (~1 - 5m length) simulating capillary and dissolution trapping under various heterogeneous conditions.
- ❑ Design **injection strategies, estimate storage capacities and efficiency** for **field-scale** geological systems by using the improved numerical tools
- ❑ The findings will meet objectives of Program research to develop technologies to cost-effectively and safely store and monitor CO<sub>2</sub> in geologic formations and to **ensure storage permanence**.
- ❑ Developed approach and technologies in this project specifically contribute to the Carbon Storage Program's effort of supporting industries' **ability to predict geologic storage capacity to within +/- 30 percent**.

# Project Overview:

## Goals and Objectives

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### □ Objectives

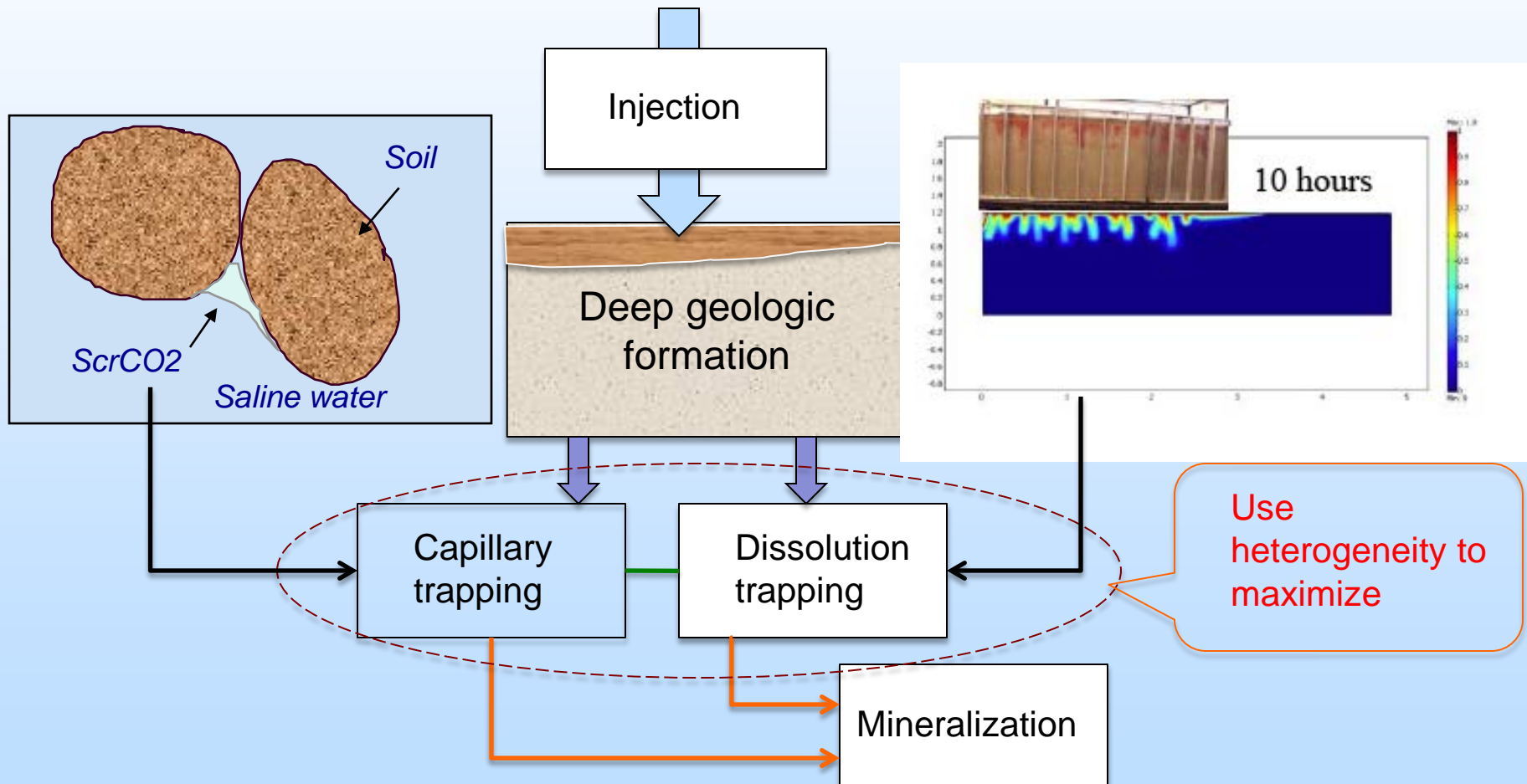
- Investigate how the trapping mechanisms are affected by **formation heterogeneity** with the ultimate goal of contributing towards improving numerical tools and **up-scaling methods** to design injection strategies, estimate storage capacities and efficiency, and conduct performance assessment for stable storage.

### □ Goals

- The mechanisms of capillary and dissolution trapping that are affected by heterogeneity will be investigated using **intermediate scale testing** in porous media tanks.
- The generated data will be used to **improve the conceptual understanding and develop and validate models** that will allow more accurate prediction of CO<sub>2</sub> fate and transport in deep geologic saline formations.

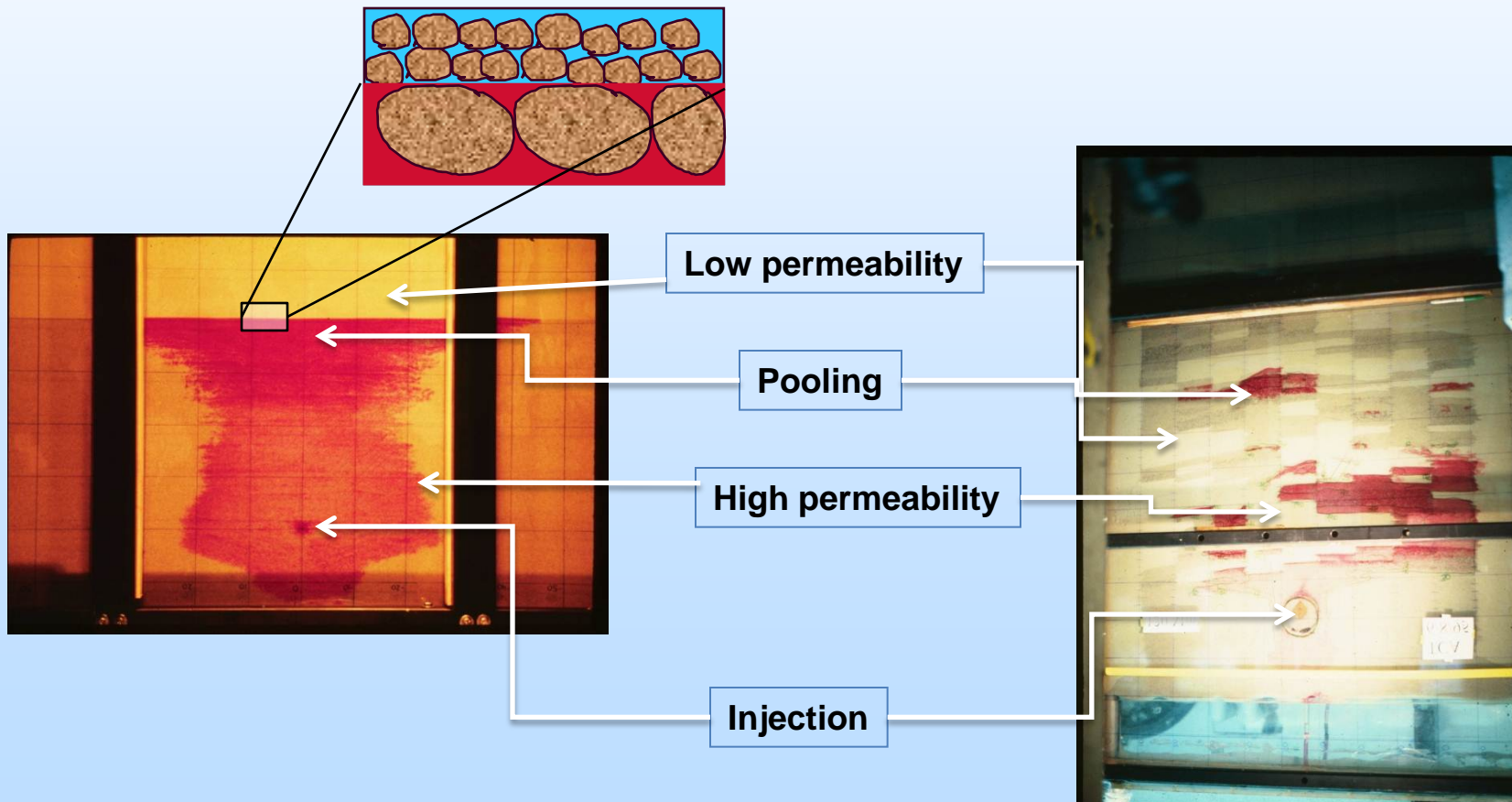
# Successful Storage

The goal of successful storage is to create stable conditions where the CO<sub>2</sub> becomes **immobilized** through **entrapment**, **dissolution**, and **mineralization**.



# Conceptualization

In naturally **heterogeneous** formations, the supercritical CO<sub>2</sub> will **preferentially migrate** into higher permeability zones and **pool under the interface** of the confining low permeability layers due to **capillary barrier effects** (very high entry pressure of the non-wetting fluid).

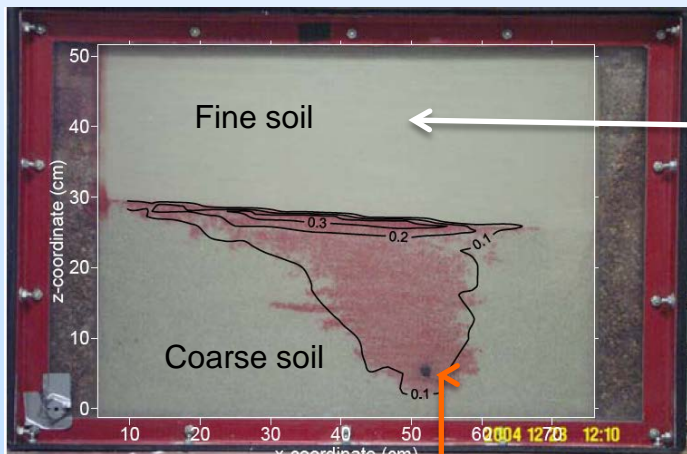


# Heterogeneity and Capillary Trapping

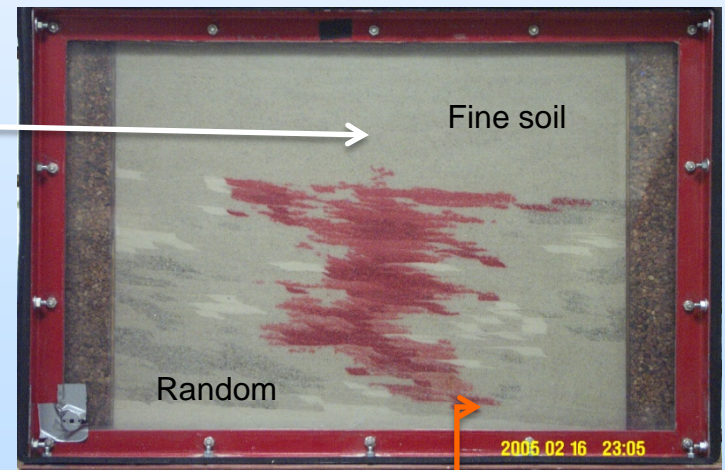
Entrapment efficiencies of  $\text{CO}_2$  (*defined as the total mass trapping per unit volume of the formation*) in relatively homogeneous and highly heterogeneous systems can be quite different.

Knowledge gaps exist on how the *heterogeneity* influences *capillary entrapment* of  $\text{ScrCO}_2$ .

Homogeneous



Heterogeneous



Cap rock

Injection



# Heterogeneity and dissolution trapping

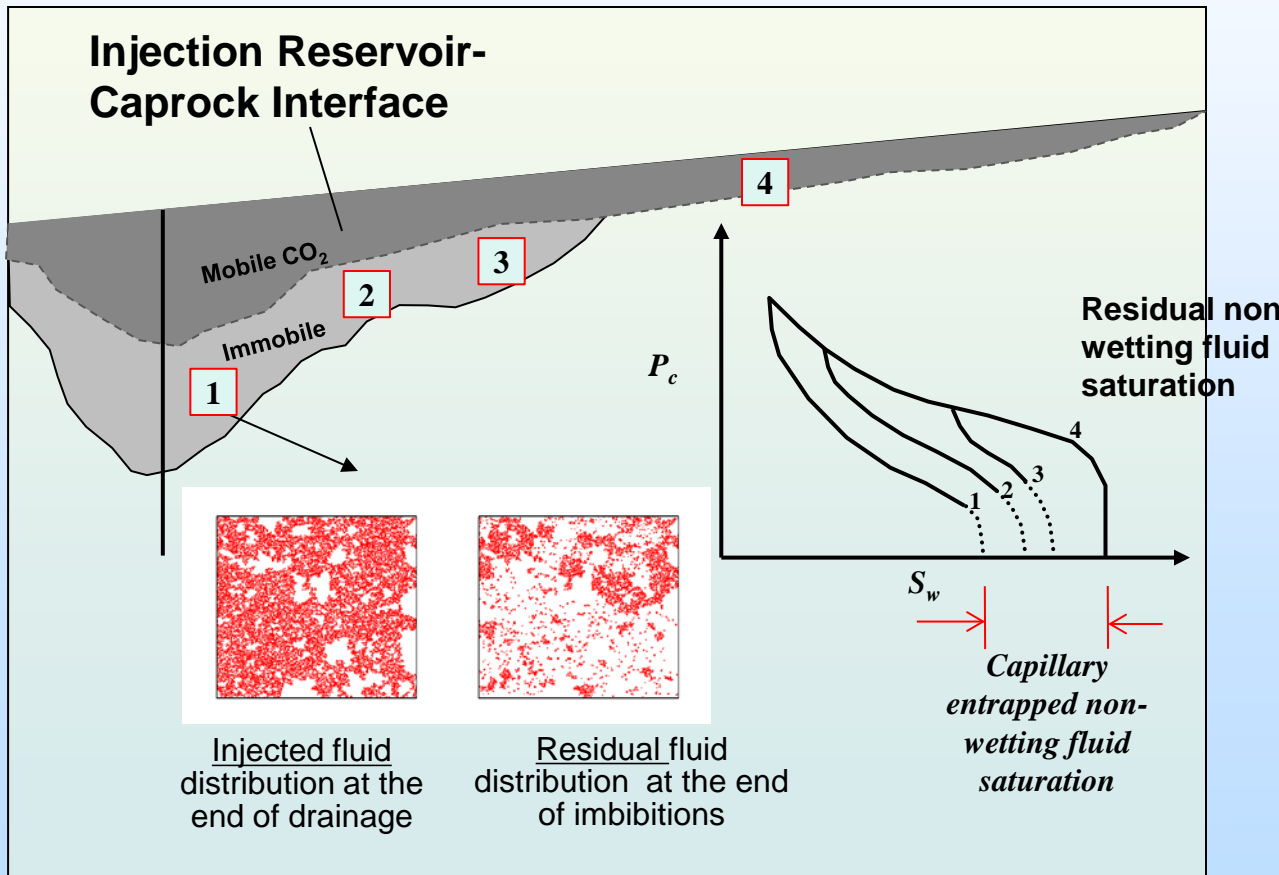
Dissolution of  $\text{CO}_2$  in **heterogeneous** systems can be enhanced due to **increases in interfacial areas** between water and supercritical  $\text{CO}_2$ .

Knowledge gaps exist on how the **heterogeneity** influences dissolution trapping of  $\text{CO}_2$ :

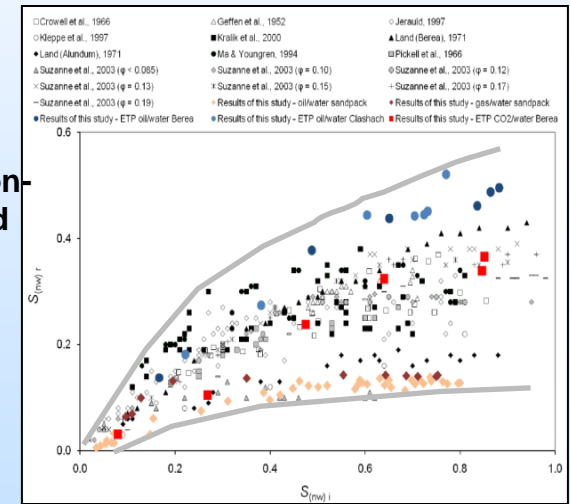


# Entrapped CO<sub>2</sub> fluid saturation after imbibition is a function of maximum saturation distribution at the end of injection.

Knowledge gap: No physically-based theory exists for representation of hysteresis in constitutive models with capillary trapping at macroscopic scale



Pentland et al. 2010, SPE



**Non-wetting fluid saturation at the end of drainage**

# Research Questions

## *Capillary Trapping*

- ❑ How do **heterogeneities and connectivity (spatial continuity of different permeability zones)** affect entrapment efficiency of **scCO<sub>2</sub>** in deep geological formations?
- ❑ How well the **existing continuum-based models and the constitutive models** capture multiphase (water/scCO<sub>2</sub>) flow behavior in deep formations?

## *Dissolution Trapping*

- ❑ What are the **effects of heterogeneity** on dissolution and **density-driven fingers**?
- ❑ Can dissolution of CO<sub>2</sub> in **heterogeneous systems** be enhanced due to increases in **interfacial areas** between water and supercritical CO<sub>2</sub>?
- ❑ How effective is diffusion into low permeability zones in enhancing trapping?
- ❑ Under what conditions **convective mixing** is important?

# Project Overview- Scope of Work

- ❑ Generate a **comprehensive data set in intermediate scale test tanks** simulating multiphase flow to investigate how effective **capillary trapping** at field scale is affected by the texture transitions and variability in **heterogeneous field formations**.
- ❑ Generate a **comprehensive data set in intermediate scale test tanks** simulating dissolution of partially miscible fluids to investigate how **effective dissolution trapping** at the field scale is affected by **heterogeneity-driven preferential flow** and cross-intra-layer mixing.
- ❑ **Modeling efforts** that includes various scenario simulations to evaluate whether the existing modeling codes can accurately capture processes observed in the test tanks. **This effort will lead to develop up-scaling methods for larger-scale applications.**

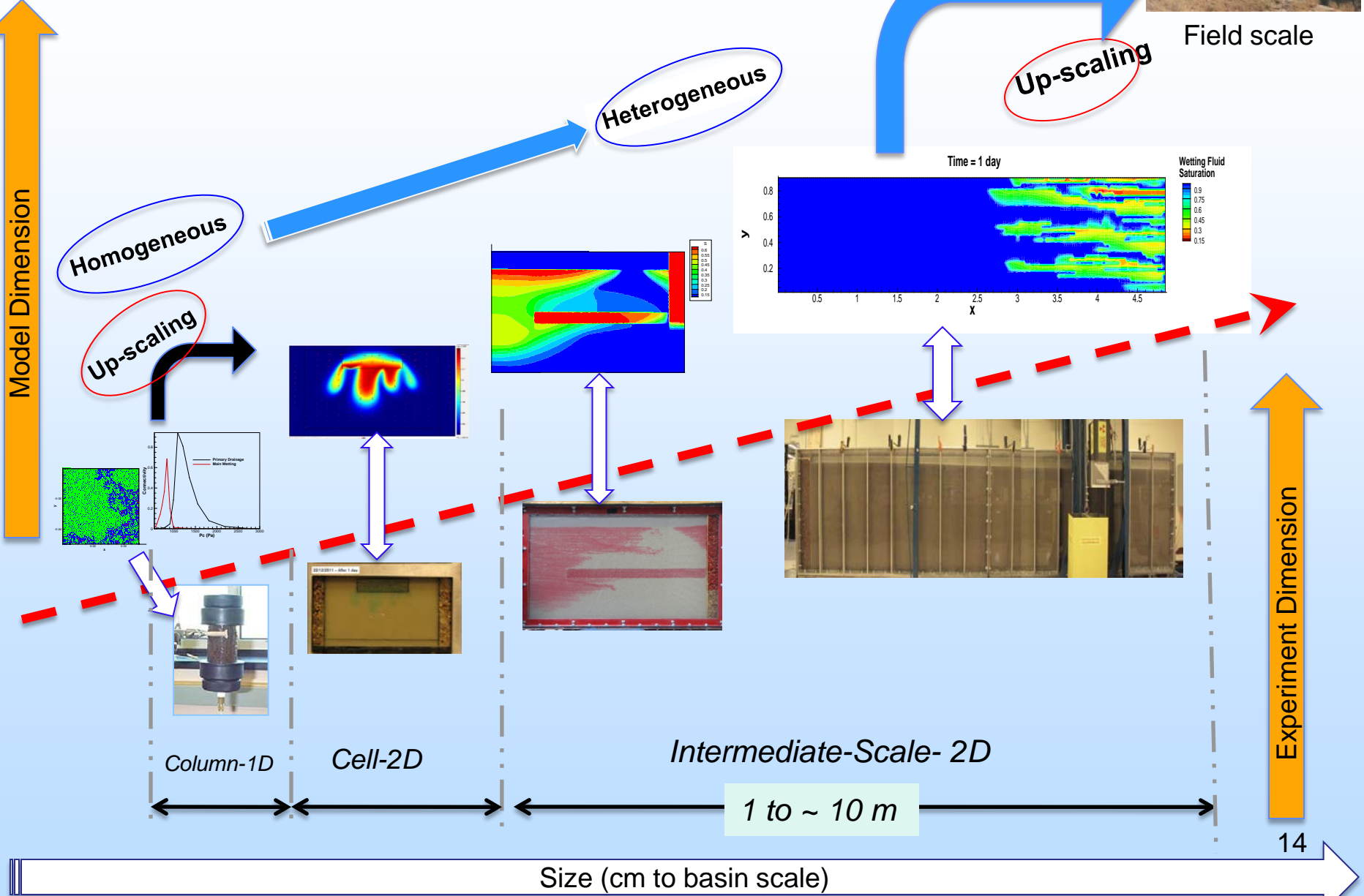
# Project Overview: Scope of Work

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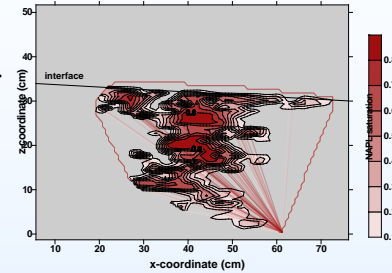
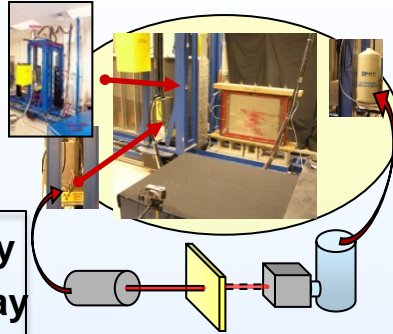
Why has the Scope of Work been defined as it is?

- ❑ Even though trapping at the core-scale is reasonably well understood and empirically modeled for relatively homogenous systems, **critical knowledge gaps exist on how these processes manifest** themselves under conditions of ubiquitous field heterogeneities to estimate or predict effective trapping capacities of field systems.
- ❑ Comprehensive understanding of the CO<sub>2</sub> storage and entrapment problem is only possible through multistage analysis comprising of **experimental studies under highly controlled conditions and modeling**.
- ❑ To our knowledge, **none of the existing modeling tools have been validated** or tested for their ability to accurately capture the CO<sub>2</sub>-brine-water flow patterns and entrapment mechanisms in porous media, specifically under heterogeneous conditions.

# Multi-scale experimental and modeling approach

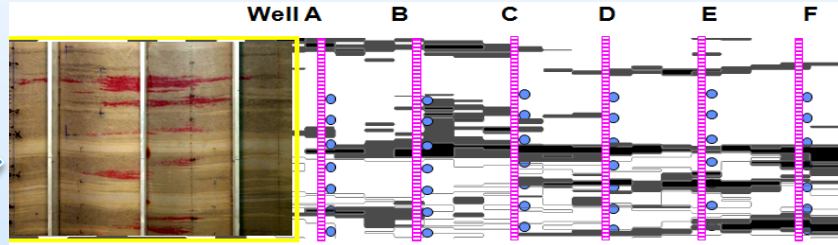


# Experimental Methods

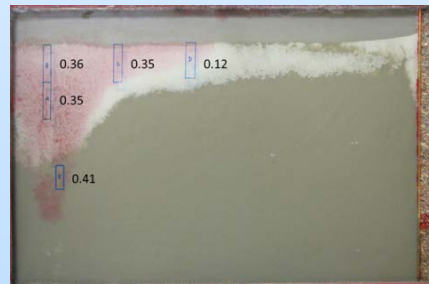


- ❑ Automated transient and spatially distributed  **saturations**  using x-ray attenuation

- ❑ Aqueous sampling to determine dissolved  **plume concentrations** , and core destructive sampling from low permeability zones



- ❑ Core destructive sampling to determine  **final entrapment saturations** .



- ❑ Measurement of multiphase  **model parameters**  (capillary pressure-saturation-relative permeability relationships)



# Selection of Surrogate Test Fluids

- Laboratory investigation of scCO<sub>2</sub> migration without high pressure in deep formations can be conducted using **analogous fluids having similar density and viscosity contrasts as scCO<sub>2</sub> – brine** phases under storage conditions

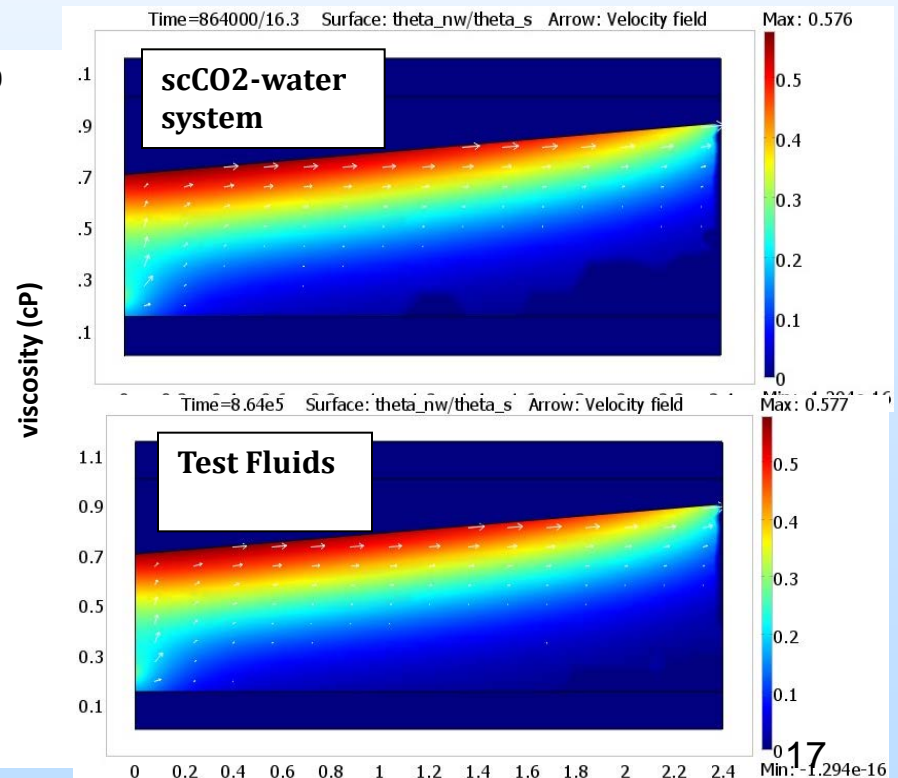
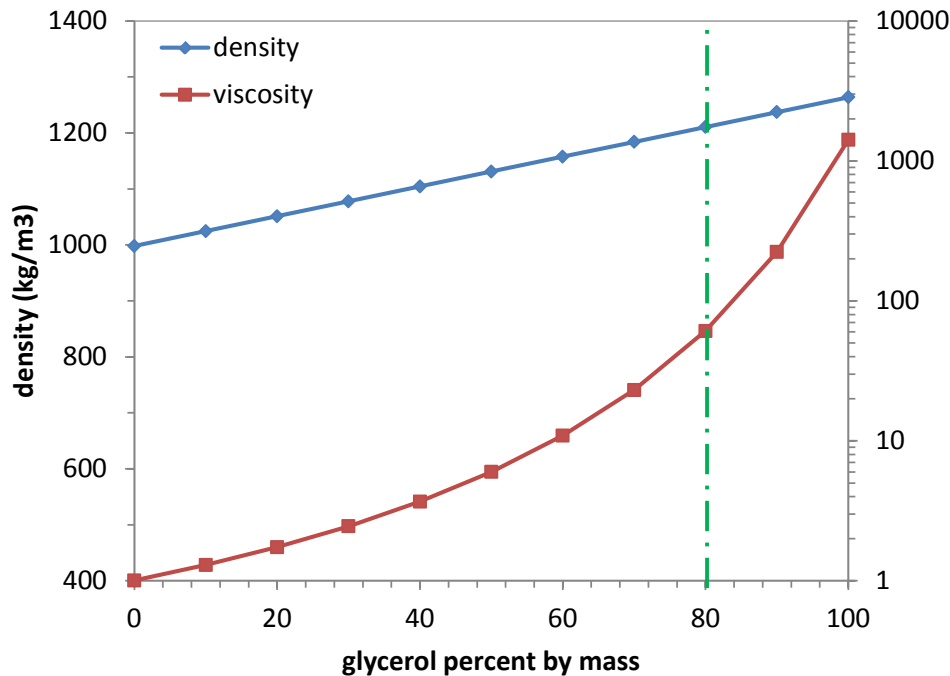
Dimensionless Numbers	scCO <sub>2</sub> -brine @ Typical Reservoir Conditions	Soltrol220-glycerol/water @ 20C, 1 atm	Water in Propylene Glycol @ 20C, 1 atm	Hexanol in Water @ 20C, 1 atm
Bond # $B_o = \frac{\Delta\rho g k}{\sigma}$	~ 10 <sup>-7</sup> - 10 <sup>-8</sup>	~10 <sup>-6</sup> - 10 <sup>-7</sup>	~10 <sup>-6</sup> - 10 <sup>-7</sup>	~10 <sup>-6</sup> - 10 <sup>-7</sup>
Capillary # $Ca = \frac{\mu_{nw} u_T}{\sigma}$	~ 10 <sup>-5</sup> - 10 <sup>-8</sup>	~10 <sup>-6</sup> - 10 <sup>-7</sup>	~10 <sup>-7</sup> - 10 <sup>-8</sup>	~10 <sup>-7</sup> - 10 <sup>-8</sup>
Viscosity Ratio $\frac{\mu_{nw}}{\mu_w}$	~ 0.05 - 0.2	~0.074	~0.017	~0.475
Density Ratio $\frac{\rho_{nw}}{\rho_w}$	~ 0.2 – 0.8	~0.66	~0.9	~0.814
Solubility	~3-5 %	immiscible	miscible	0.6%



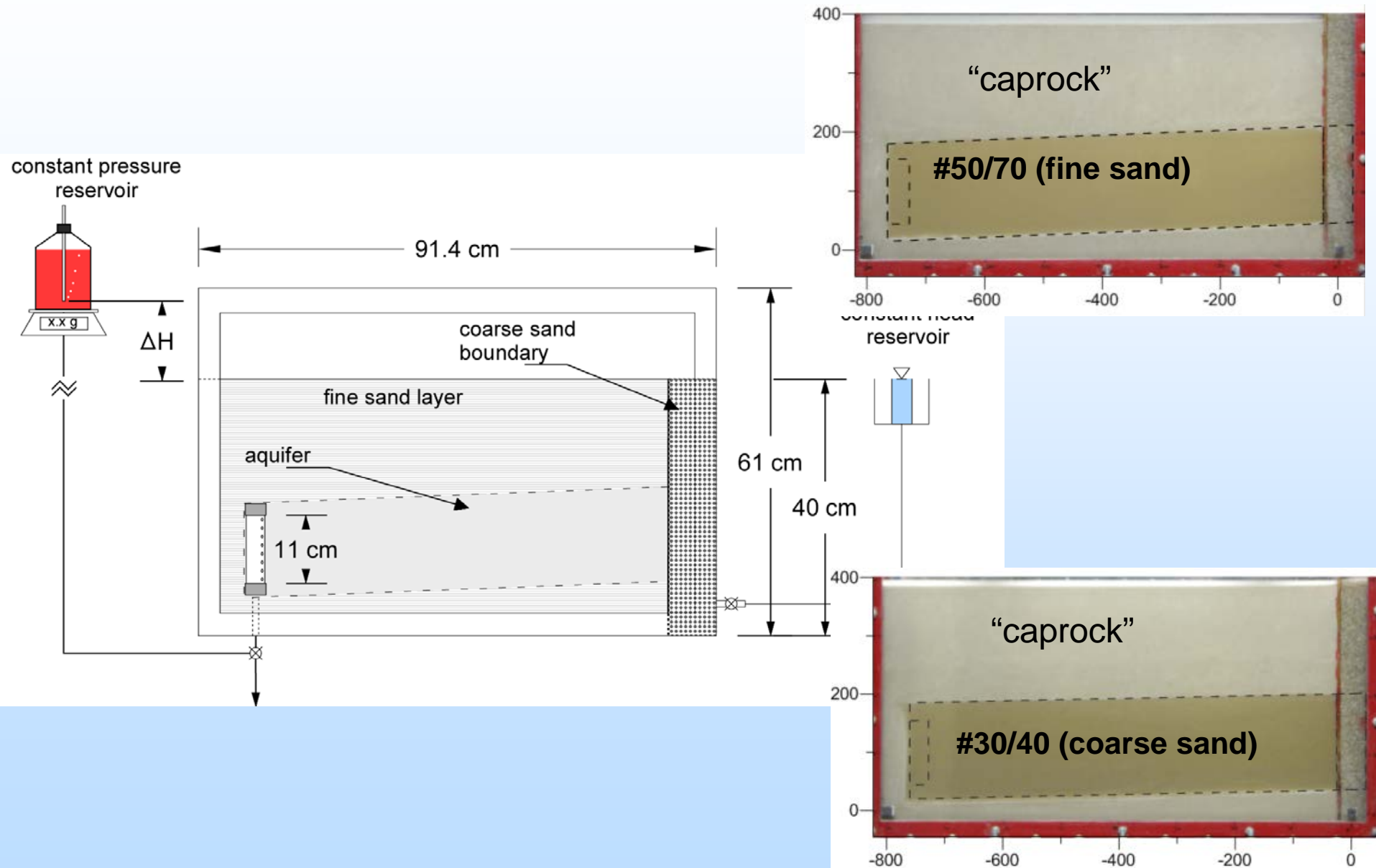
# Numerical Validation of Scaling Approach

- Identical results can be obtained if the **same dimensionless numbers** are chosen for the geometrically similar two systems (Shook et al., 1992; Gharbi et al., 1998).

*Glycerol/water mixture at ambient conditions*



# Experiments on trapping in homogeneous systems

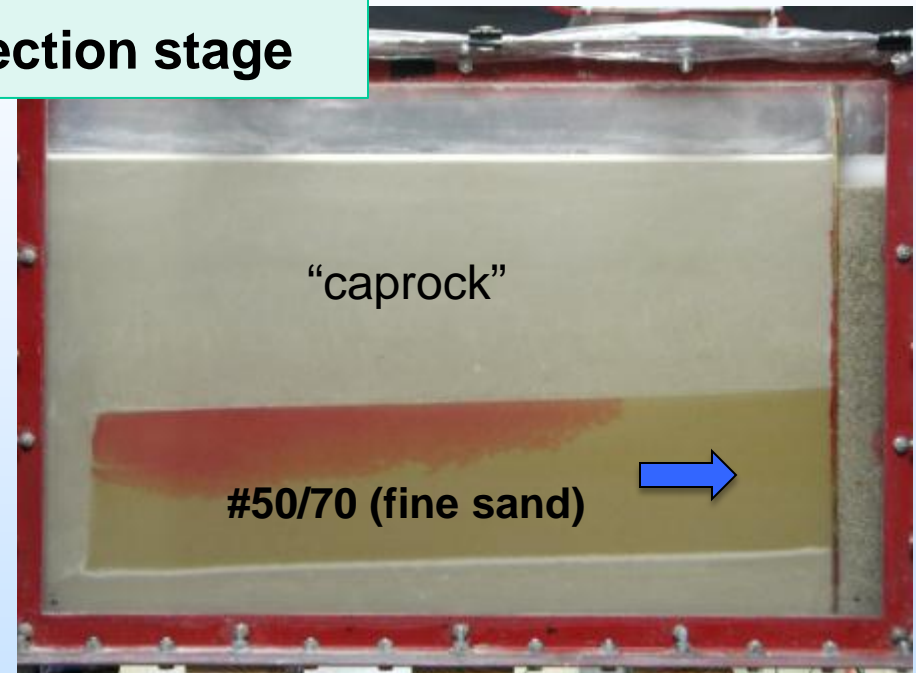
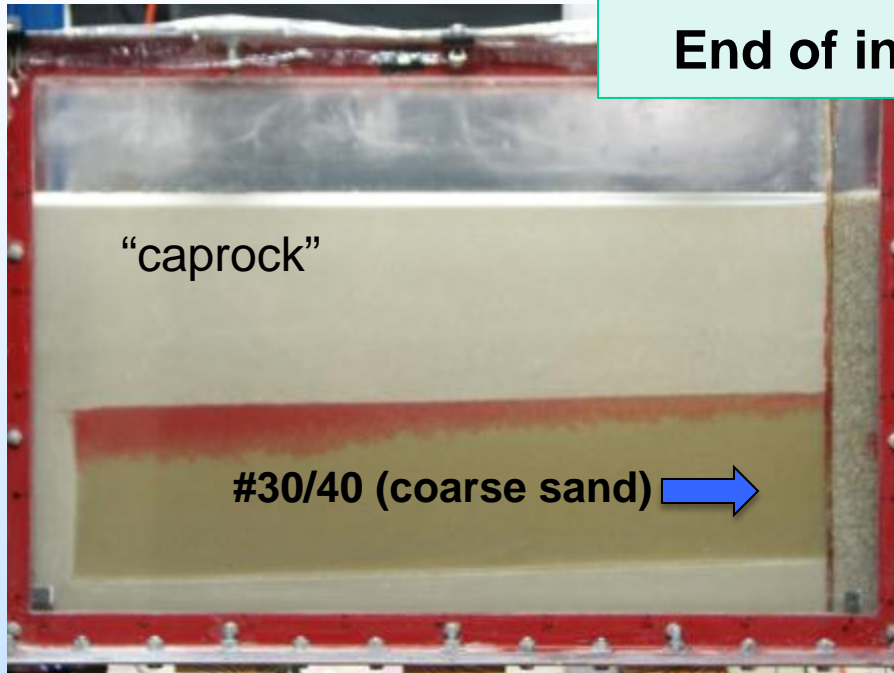


# Sweep efficiency related to Bond Number

Max swept volume ~20%

Max swept volume ~30%

End of injection stage



$Bo = 5.86E-05$

Buoyancy forces

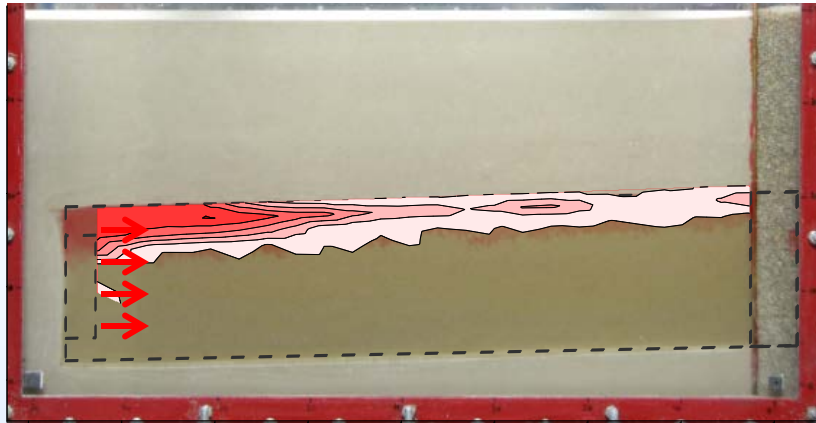


$Bo = 9.30E-06$

$$Bo = \frac{\Delta\rho g k}{\sigma}$$

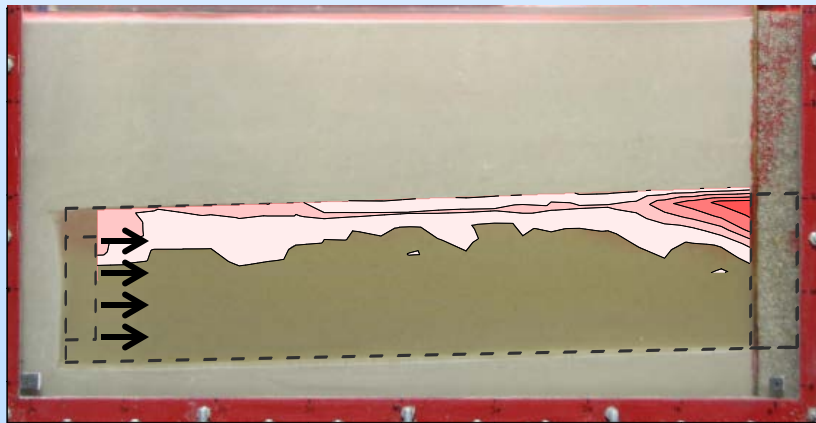
# Experiment 1: #30/40 saturation measurement

*1 hr 47 min*



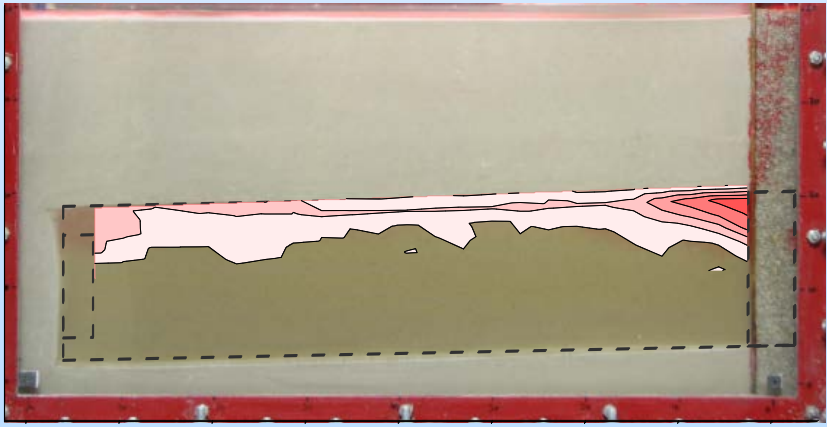
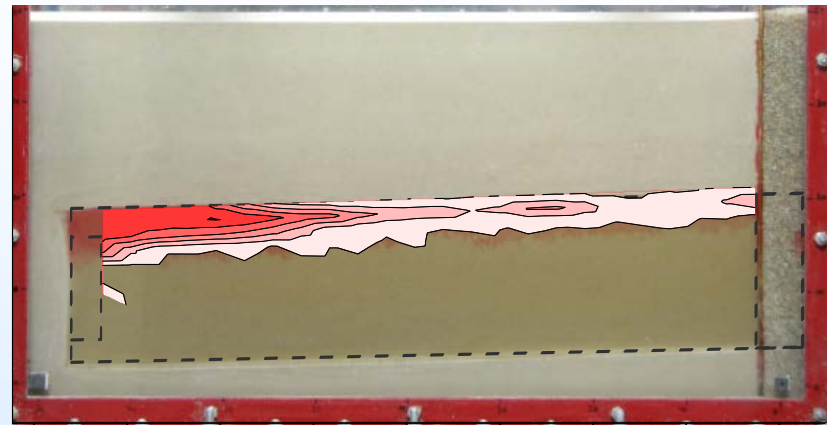
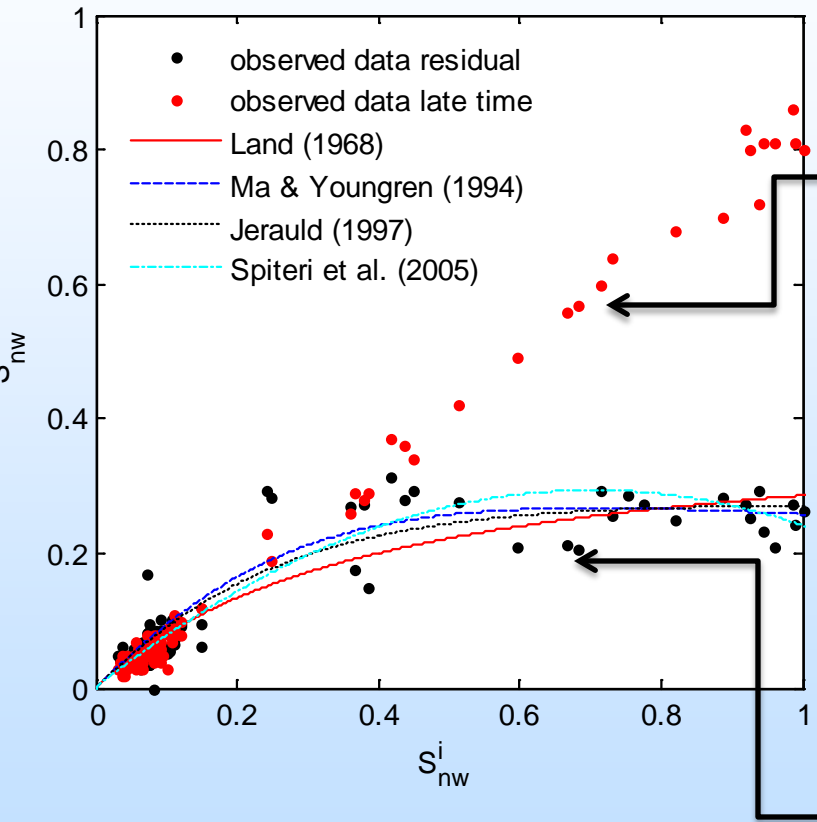
Plume distribution at late time (injection stopped at  $t = 5\text{hr}$ )

*607 hr 46 min*



Plume footprint at residual saturation after **sweeping**

# Initial-Residual saturation vs final trapping after sweep

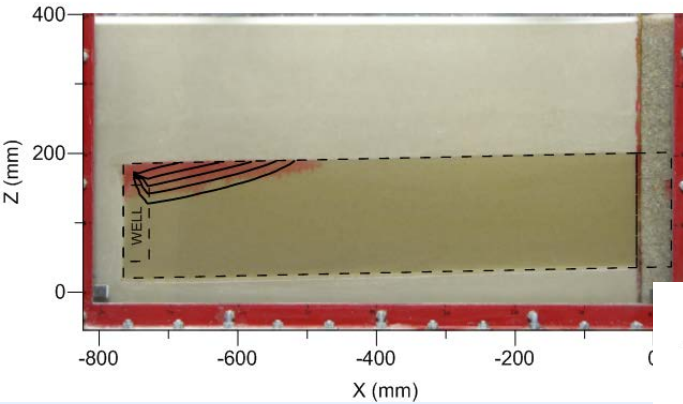


Similar results found by Fagerlund et al.,  
*Vadose Zone Journal*, 2006

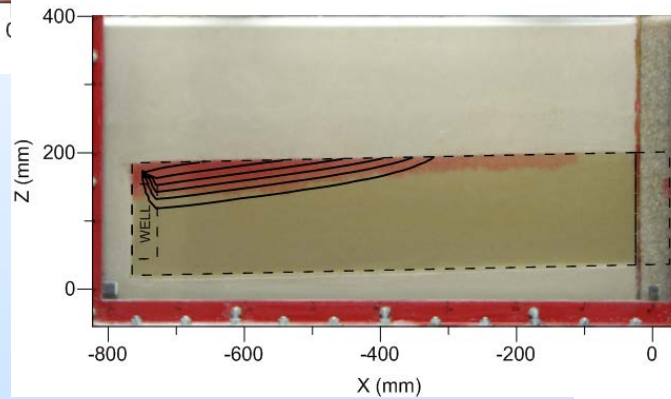
# TOUGH2-T2VOC simulations with analog fluids

**1 hr 33 min**

t = 1hr 33min

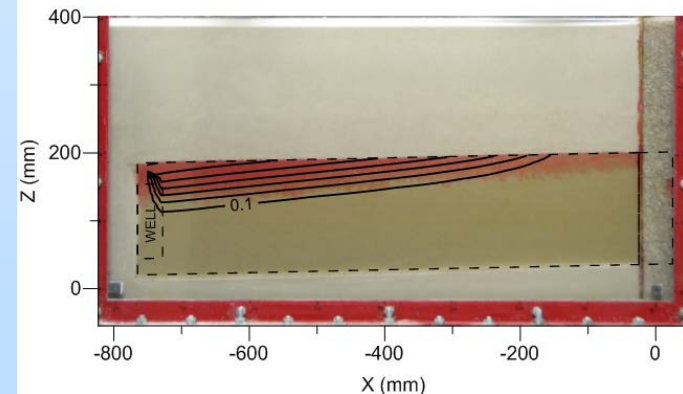


t = 3hr 34min



**5 hr 30 min**

t = 5hr 30min



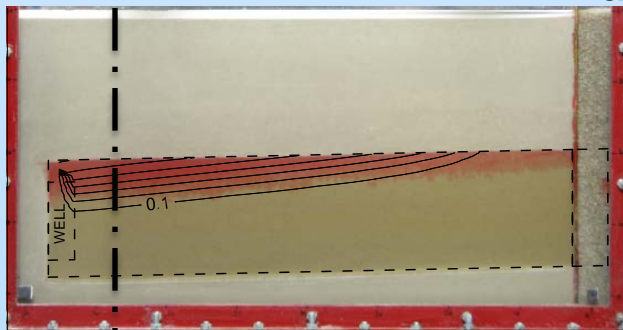
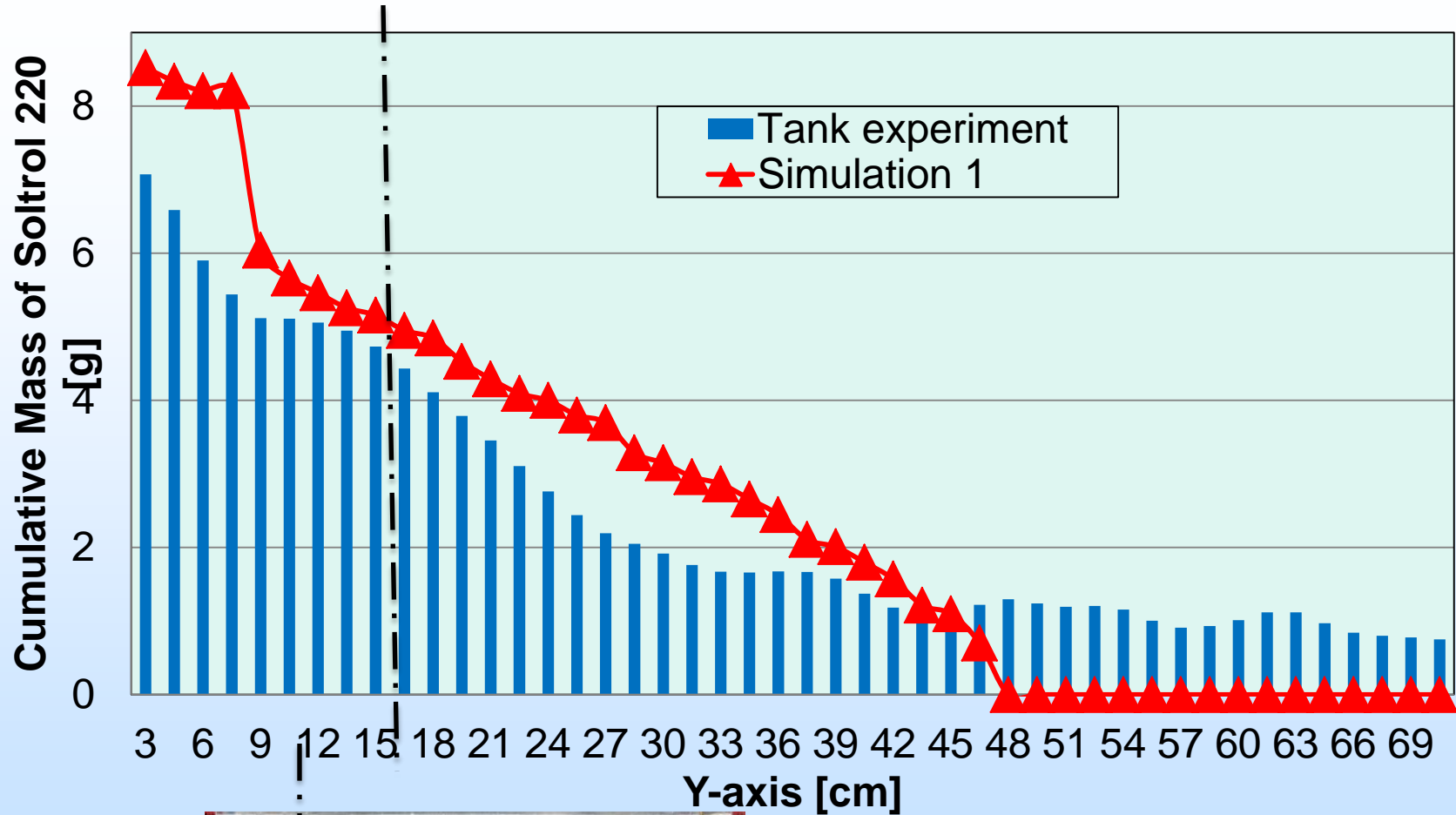
T=20°C, P= 80 kPa

$\rho_{\text{Soltrol}} = 860 \text{ kg/m}^3$ ,  $\rho_{\text{glycerol/water}} = 1210 \text{ kg/m}^3$

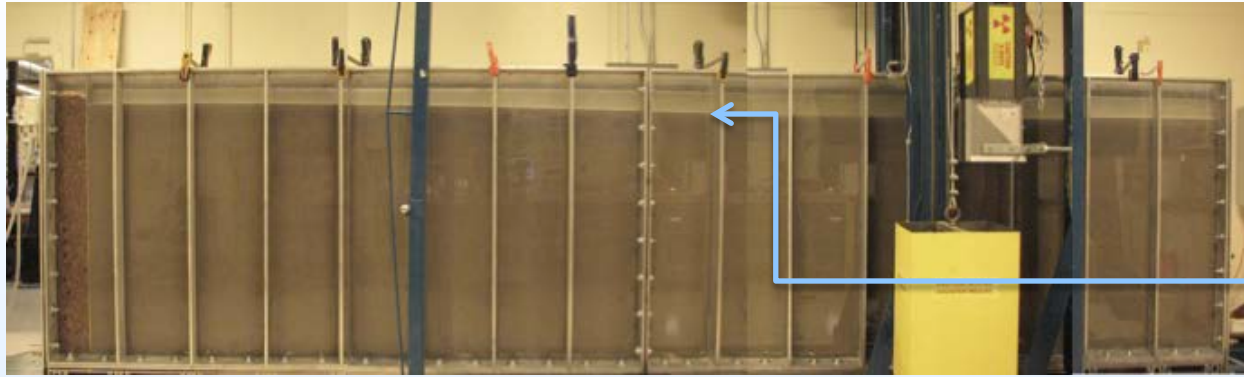
$\mu_{\text{Soltrol}} = 4.5 \text{ mPa}\cdot\text{s}$ ,  $\mu_{\text{glycerol/water}} = 61 \text{ mPa}\cdot\text{s}$

Q = 0.71 ml/min, t = 5.5 h,  $V_{\text{inj}} = 240 \text{ ml}$

# TOUGH2-T2VOC modeling comparison to experiments



# Design and assembly of large tanks



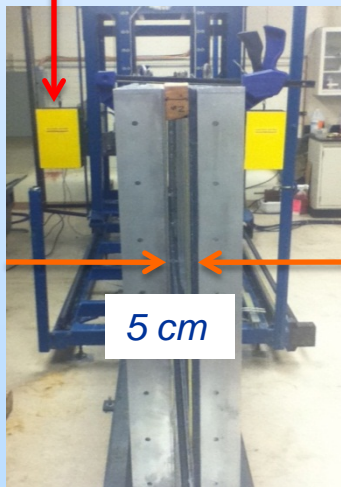
Sloping capping layer

16 ft

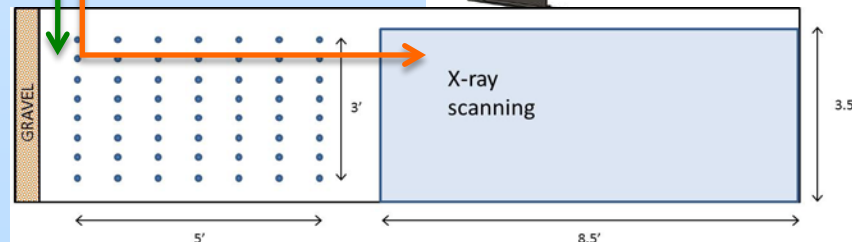
4 ft

X-ray attenuation  
For phase saturation  
measurement

Ports for  
aqueous  
sampling



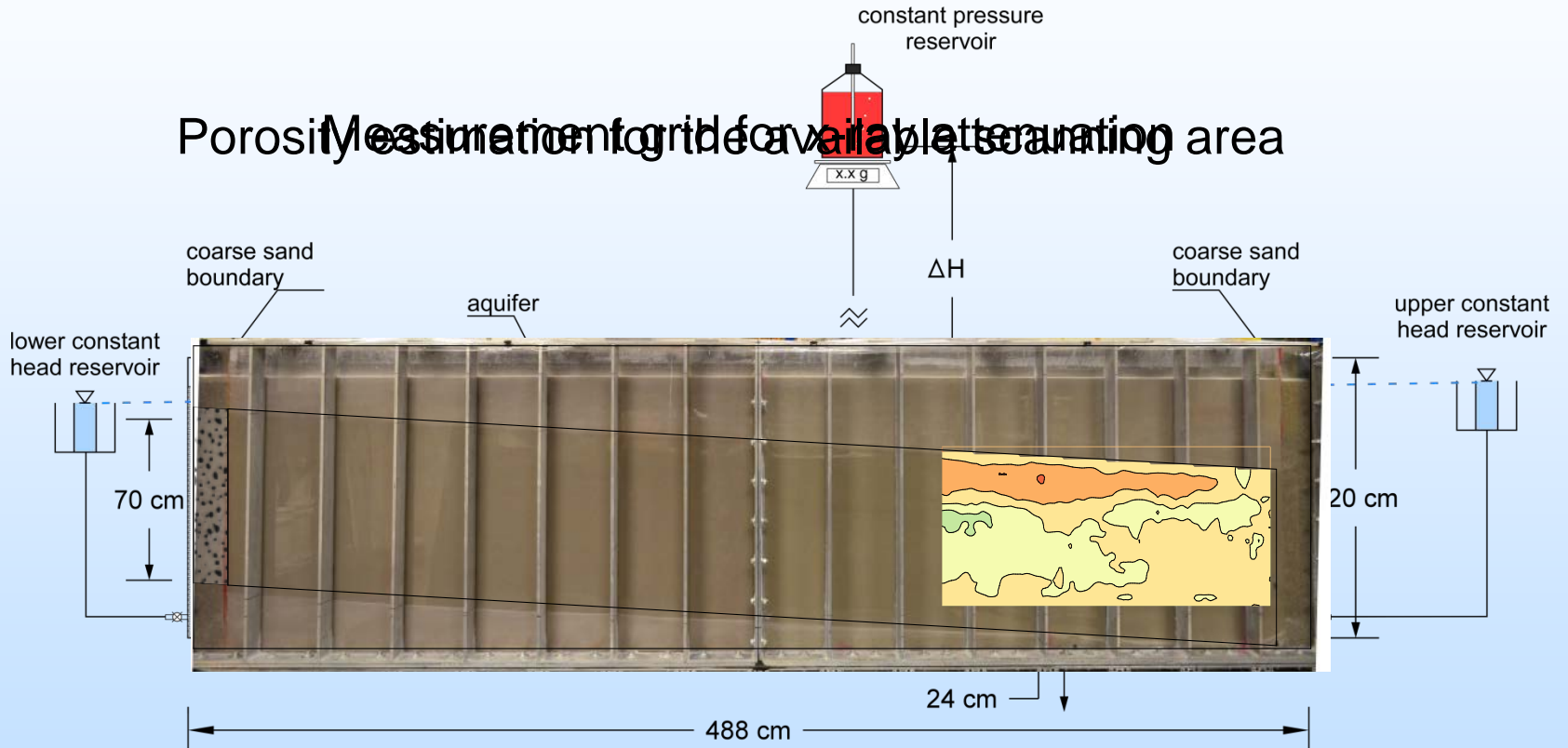
5 cm





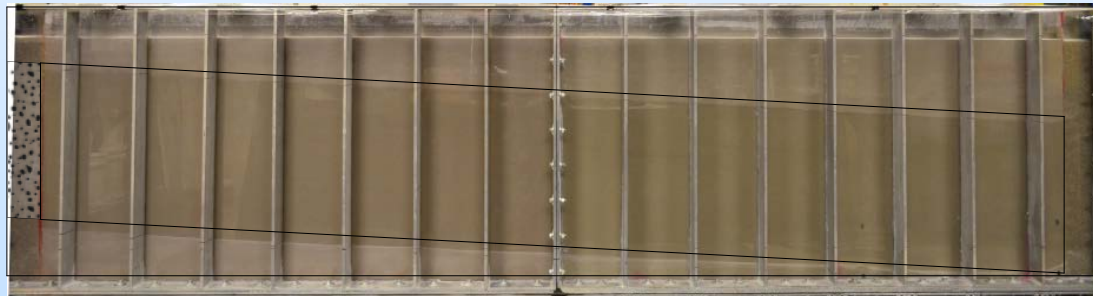
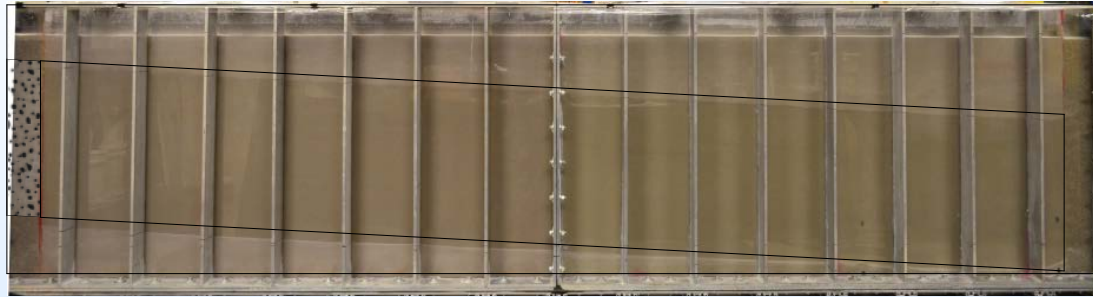
# Large tank experiment

Porosity Measurement grid for available planar scanning area



# Modeling analog fluids with TOUGH2-T2VOC

Injection stage lasts 6 hours @ 6 ml/min  
Redistribution simulated for 10 days



## 20.2 hrs of simulation for 10.4 hrs of injection



- ✓ Injection volume = 890 ml
- ✓ Injection flow rate = 1.43 ml/min (average)

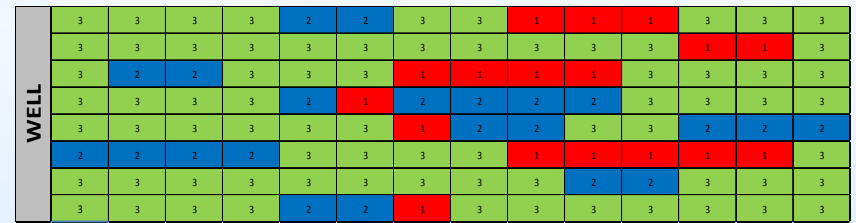
# Entrapment saturation distribution (3 days after injection)

# Tank Experiments in Highly Heterogeneous Systems

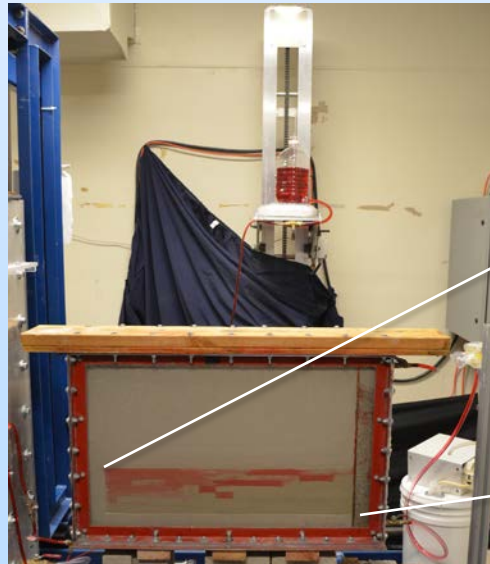
*A computer-generated realistic heterogeneous aquifer*



*Simplified for packing*



Tank data

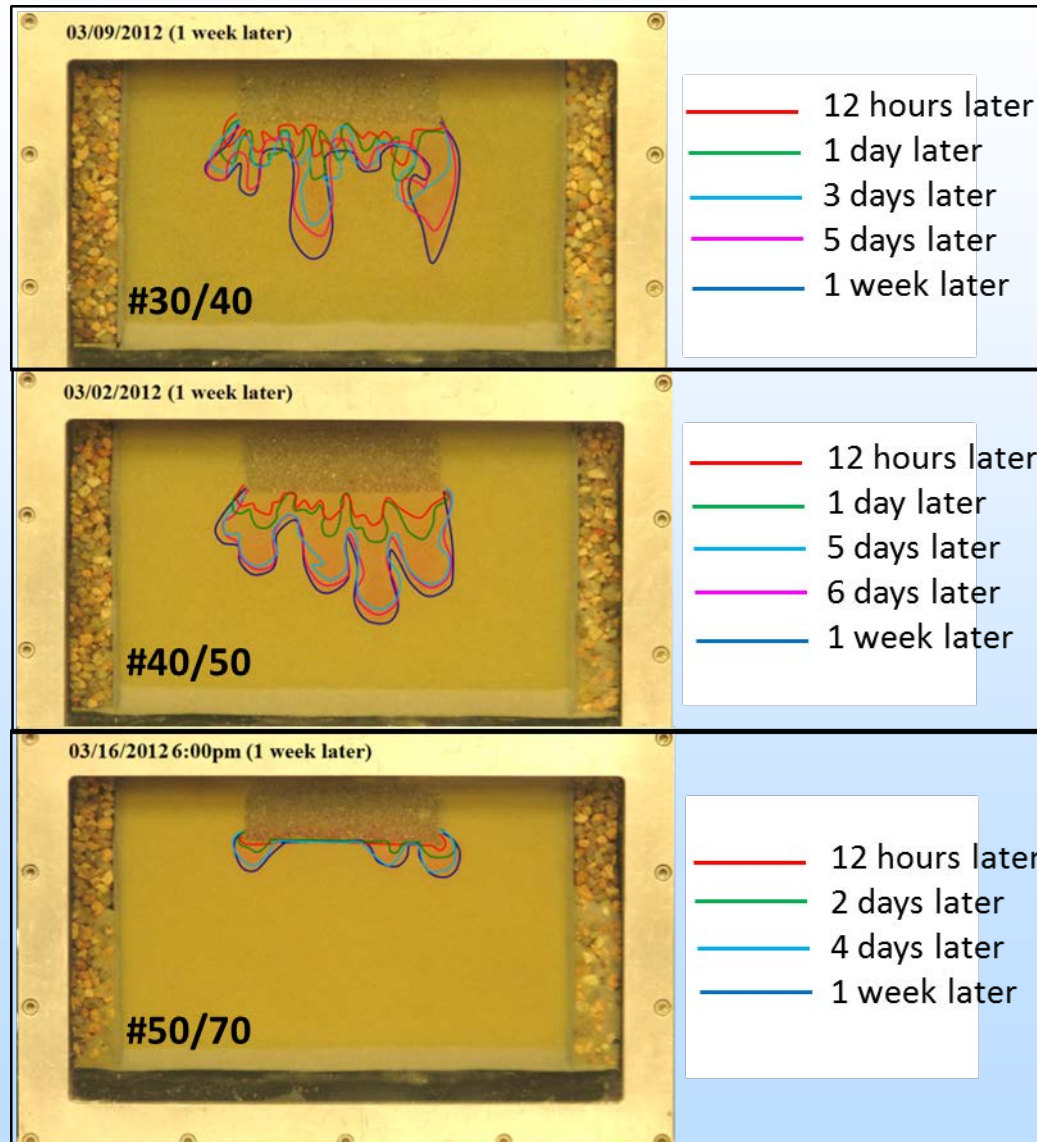
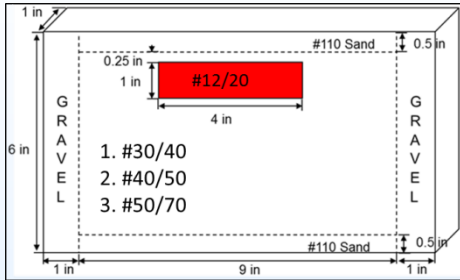


Tank setup

# Dissolution trapping

- ❑ Selection of analog fluids
- ❑ Small cell experiments
- ❑ Convective mixing
- ❑ Dissolution model development
- ❑ Large tank experiments (dissolution and low permeability zone storage)

# 2-D Small Tank Experiments: Homogeneous Media (water/propylene glycol )



Ra

451

221

138

Rayleigh  
Number, Ra

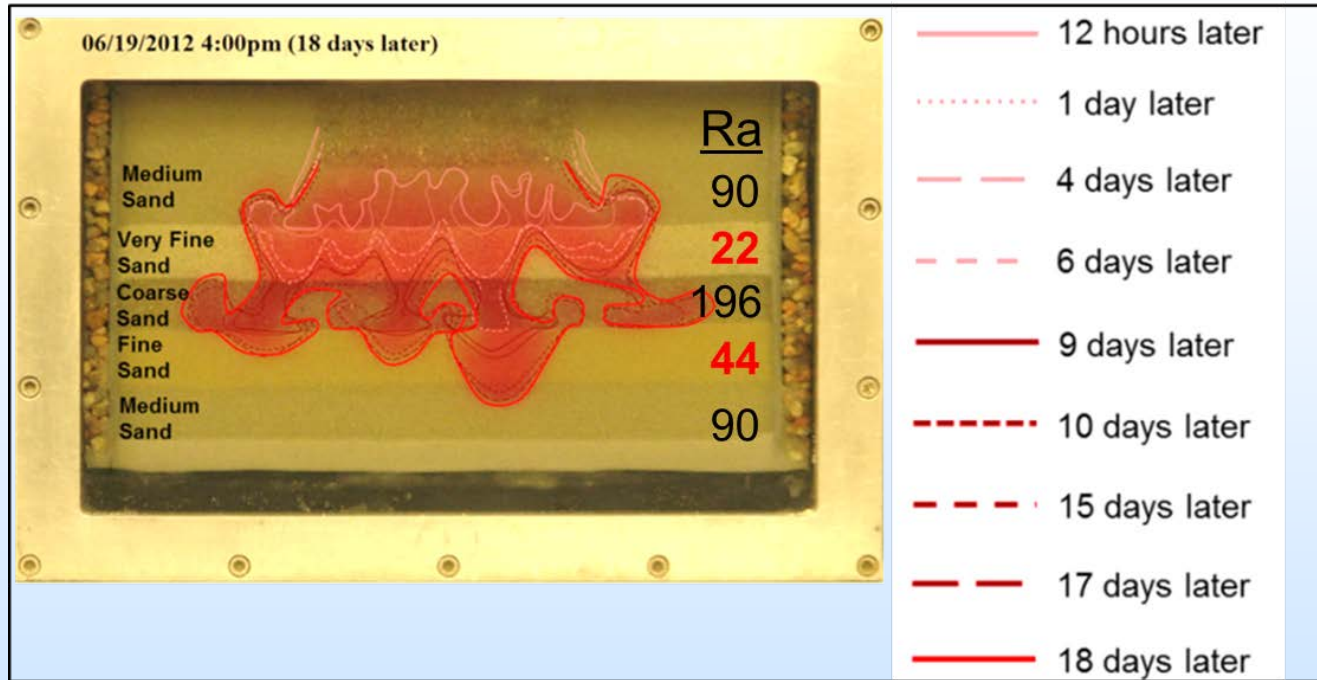


$$Ra = \frac{k\Delta\rho gH}{D\mu\phi}$$

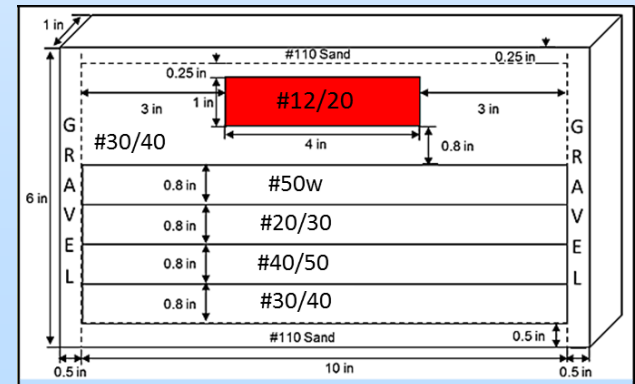
$$Ra_c > 4\pi^2 (\sim 40)$$

Rayleigh Number for  
*scrCO2*-brine @  
Typical Reservoir  
Conditions  
 $\sim 6 - 10^3$

# 2-D Small Tank Experiments: Heterogeneity effect on density-driven fingering (water/propylene glycol )

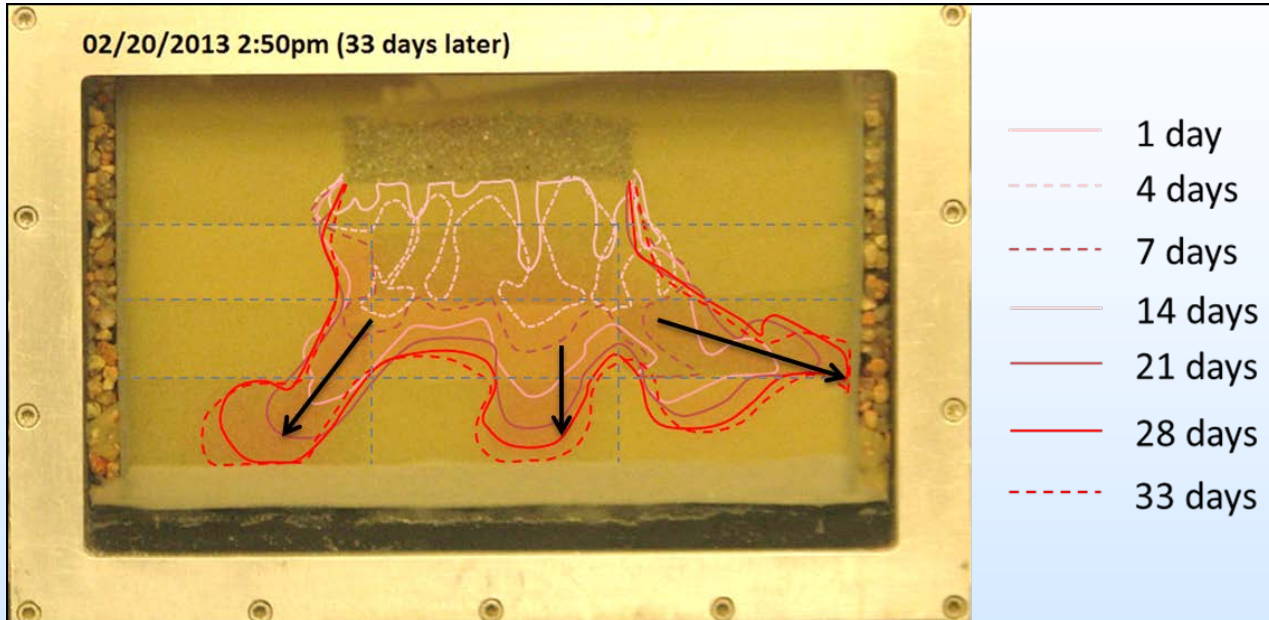


In the transition of high-permeable medium and low permeable medium, **characteristics of fingered flow** tends to change due to **merging of fingers**

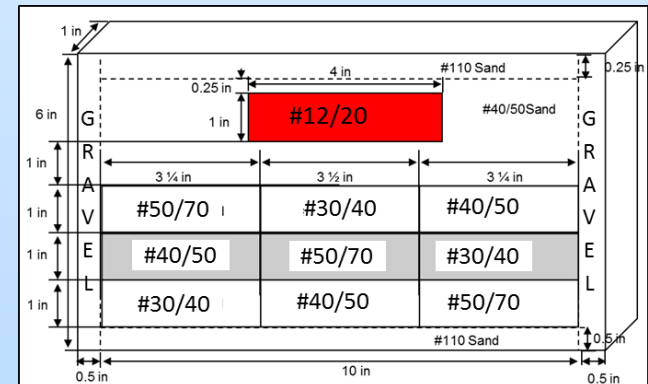




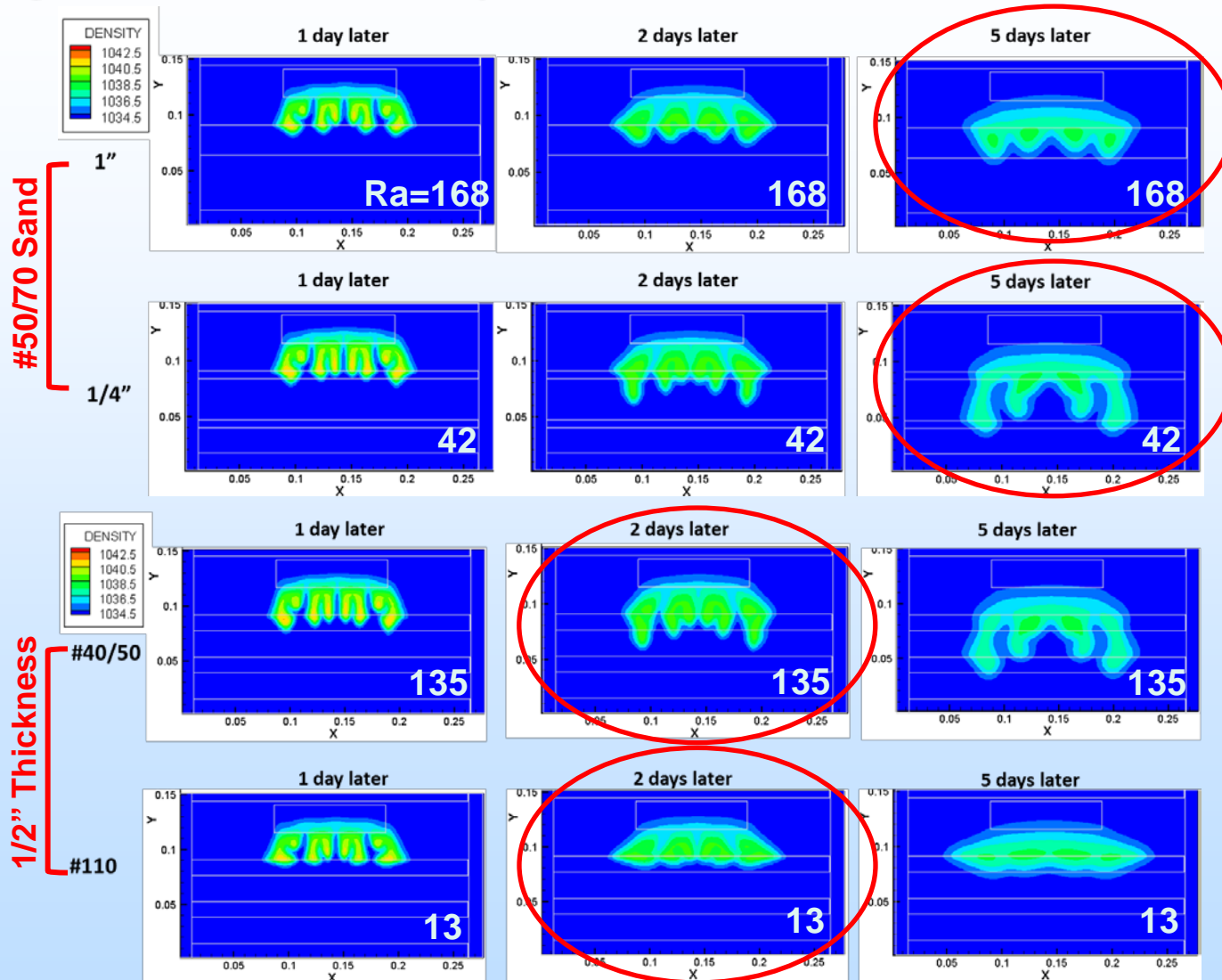
# 2-D Small Tank Experiments: Heterogeneity effect on density-driven fingering (water/propylene glycol )



Convective mixing controlled by density driven sinking through **high permeability connected pathways**



# Numerical Modeling: Layered Heterogeneous Formations having Low Permeability Zones



Rayleigh Number for *scrCO2*-brine @ Typical Reservoir Conditions  $\sim 6 - 10^3$

# Accomplishments

- ❑ Task 2 – Experiments in intermediate-scale
  - ✓ Selected and tested surrogate fluids
  - ✓ Small tank experiments completed for testing capillary trapping and density-dependent fingers in homogeneous and simple heterogeneous systems
  - ✓ Initiated large tank experiments for capillary trapping
- ❑ Task 3 – Modeling
  - ✓ Simulated the two-phase flow in small tank experiments and compared the model results with experimental data
  - ✓ Developed a new multiphase flow solver (based on the Finite Volume method) for analysis of the experimental data and new constitutive models and non-equilibrium mass transfer
  - ✓ Developed a new code for analyzing heterogeneity: Computes connectivity based on invasion percolation algorithm. This code also involves algorithms to upscale two-phase flow parameters.
  - ✓ Developed a new hysteresis model and tested against few data sets

# Findings

- ❑ The numerical models based on the classical two-phase flow theory were able to capture the main features observed during the migration of the **ScCO<sub>2</sub> surrogate** fluid in the small tanks
- ❑ Selection of appropriate **relative permeability curves** was critical to predict dynamic changes in the surrogate fluid distributions
- ❑ Incorporating **hysteresis effects** into the numerical models required for accurate prediction of post-injection capillary entrapment.
- ❑ Intermediate-scale heterogeneity (existence of lower and higher permeability zones) **enhances the capillary entrapment** in intermediate-scale.
- ❑ **Convective mixing** due to density-driven finger flow in highly heterogeneous formations **appears to be not important.**
- ❑ Our experimental results and literature show that the residual non-wetting phase saturation is strongly function of the **saturation at the end of injection.**

## Future Efforts

- ❑ **Obtain more quantitative data on temporal and spatial saturation changes using the X-ray system.**
- ❑ **Complete measurements of relative permeability of the sands in separate homogeneous column tests.**
- ❑ **Intermediate-scale heterogeneous experiments and models involving both capillary and dissolution trapping.**
- ❑ **Update model parameters with measured relative permeability curves in separate homogeneous column tests.**
- ❑ **Continue developing/testing the constitutive models with hysteresis against experimental data.**
- ❑ **Improve the numerical models by incorporating the validated constitutive models**

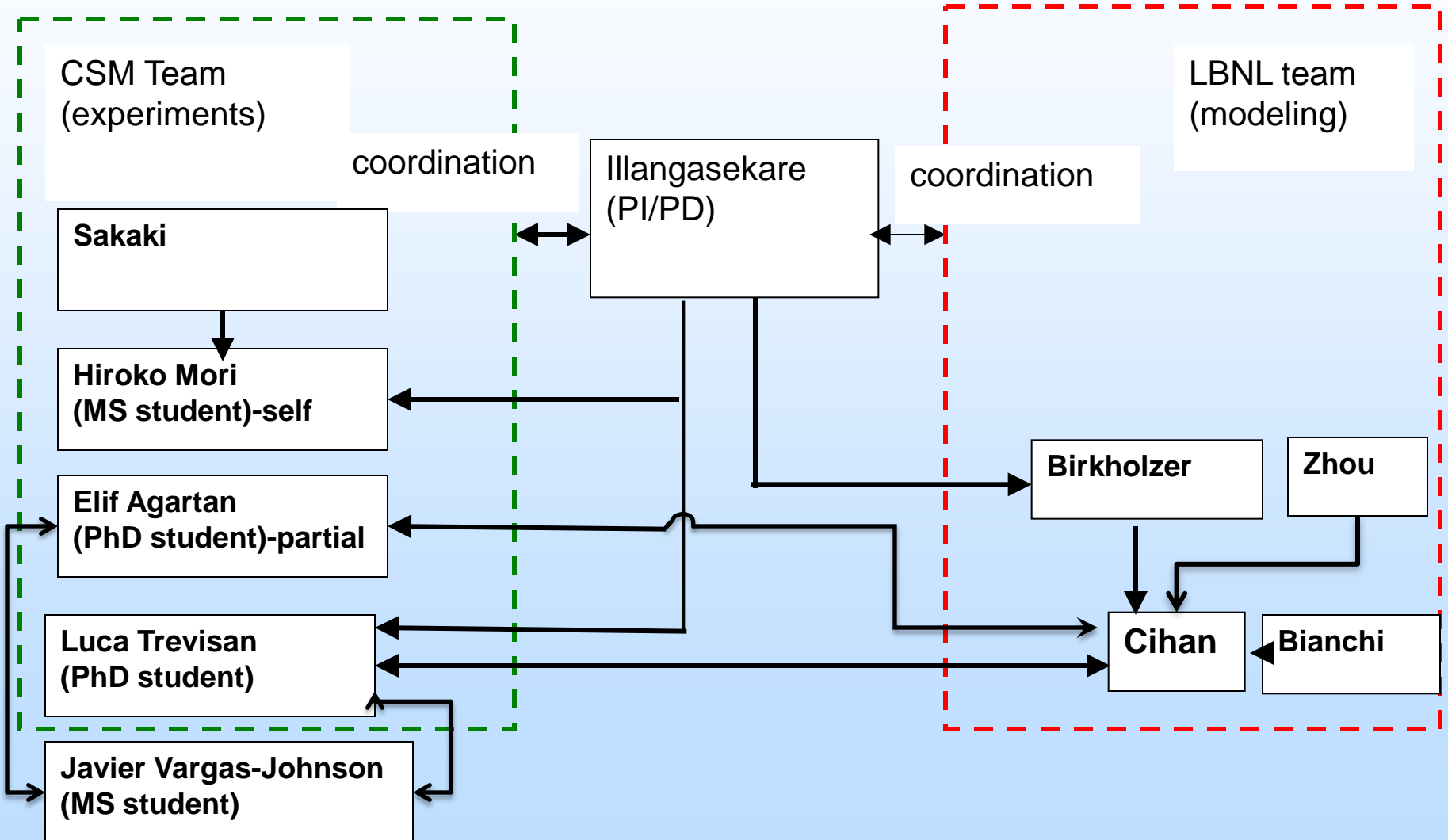
# Appendix

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- These slides will not be discussed during the presentation, **but are mandatory**

# Organization Chart

1. Scientific & Technical Merit
2. Existence of Clear, Measurable Milestones
3. Utilization of Government Resources
4. **Technical Approach**
5. Rate of Progress
6. Potential Technology Risks Considered
7. Performance and Economic Factors
8. Anticipated Benefits, if Successful
9. Technology Development Pathways



# Project Overview: Schedule

November 2010

August 2013



Task	BP 1	BP 2	BP 3
<b>Tank assembly and setup</b> <i>(Task 2.2 &amp; 2.2)</i>			
<b>Experimental methods</b> <i>(Tasks 2.1 &amp; 2.2)</i>			
<b>Homogenous immiscible</b> <i>(Tasks 2.1 &amp; 2.2)</i>			
<b>Homogenous miscible</b> <i>(Tasks 2.1 &amp; 2.2)</i>			
<b>Heterogeneous immiscible</b> <i>(Tasks 2.1 &amp; 2.2)</i>			
<b>Heterogeneous miscible</b> <i>(Tasks 2.1 &amp; 2.2)</i>			
<b>Modeling</b> <i>(Task 3)</i>			



# Bibliography

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- Cihan, A., Birkholzer, J., Illangasekare, T. H., Zhou, Q., “A Theoretical Approach to Represent Hysteresis in Capillary Pressure-Saturation Relationship Based on Fluid Connectivity in Void Space”, submitted to Water Resources Research.
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